Two-dimensional, homogeneous, isotropic fluid turbulence with polymer additives

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We carry out the most extensive and high-resolution direct numerical simulation, attempted so far, of homogeneous, isotropic turbulence in two-dimensional fluid films with air-drag-induced friction and with polymer additives. Our study reveals that the polymers (a) reduce the total fluid energy, enstrophy, and palinstrophy, (b) modify the fluid energy spectrum both in inverse- and forward-cascade régimes, (c) reduce small-scale intermittency, (d) suppress regions of large vorticity and strain rate, and (e) stretch in strain-dominated regions. We compare our results with earlier experimental studies and propose new experiments.

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I. INTRODUCTION

Polymer additives have remarkable effects on turbulent flows: in wall-bounded flows they lead to drag reduction [1, 2]; in homogeneous, isotropic turbulence they give rise to dissipation reduction, a modification of the energy spectrum, and a suppression of smallscale structures [3–13]. These effects have been studied principally in three-dimensional (3D) flows; their twodimensional (2D) analogs have been studied only over the past decade in experiments [14–16] on and direct numerical simulations (DNSs) [17–20] of fluid films with polymer additives. It is important to investigate the differences between 2D and 3D fluid turbulence with polymers because the statistical properties of fluid turbulence in 2D and 3D are qualitatively different [21]: the inviscid, unforced 2D Navier-Stokes (NS) equation admits more conserved quantities than its 3D counterpart; one consequence of this is that, from the forcing scales, there is a flow of energy towards large length scales (an inverse cascade) and that of enstrophy towards small scales (a forward cascade). We have, therefore, carried out the most extensive and high-resolution DNS study of homogeneous, isotropic turbulence in the incompressible, 2D NS equation with air-drag-induced friction and polymer additives, described by the finitelyextensible-nonlinear-elastic-Peterlin (FENE-P) model for the polymer-conformation tensor. We find that the inverse-cascade part of the energy spectrum in 2D fluid turbulence is suppressed by the addition of polymers. We show, for the first time, that the effect of polymers on the forward-cascade part of the fluid energy spectrum in 2D is (a) a slight reduction at intermediate wave numbers and (b) a significant enhancement in the large-

wave-number range, as in 3D; the high resolution of our simulation is essential for resolving these spectral features unambiguously. In addition, we find dissipationreduction-type phenomena [7, 8]: polymers reduce the total fluid energy and energy- and mean-square-vorticityor enstrophy-dissipation rates, suppress small-scale intermittency, and decrease high-intensity vortical and straindominated régimes. Our probability distribution functions (PDFs) for σ^2 and ω^2 , the squares of the strain rate and the vorticity, respectively, agree qualitatively with those in experiments [16]. We also present PDFs of the Okubo-Weiss parameter $\Lambda = (\omega^2 - \sigma^2)/8$, whose sign determines whether the flow in a given region is vortical or strain-dominated [22, 23], and PDFs of the polymer extension; and we show explicitly that polymers stretch preferentially in strain-dominated regions.

The remaining part of this paper is organized as follows. In Sec. II we define the equations we use for polymer additives in a fluid and we describe the numerical methods we use to study these equations. Section III is devoted to the results of our study and Sec. IV contains a discussion of our principal results.

II. MODEL AND NUMERICAL METHODS

The 2D incompressible NS and FENE-P equations can be written in terms of the stream-function ψ and the vorticity $\boldsymbol{\omega} = \nabla \times \mathbf{u}(\mathbf{x}, t)$, where $\mathbf{u} \equiv (-\partial_y \psi, \partial_x \psi)$ is the fluid velocity at the point \mathbf{x} and time t, as follows:

$$D_t\omega = \nu \nabla^2 \omega + \frac{\mu}{\tau_P} \nabla \times \nabla [f(r_P)\mathcal{C}] - \alpha \omega + F_\omega; \quad (1)$$

$$\nabla^2 \psi = \omega; \tag{2}$$

$$D_t \mathcal{C} = \mathcal{C}.(\nabla \mathbf{u}) + (\nabla \mathbf{u})^T \mathcal{C} - \frac{f(r_P)\mathcal{C} - \mathcal{I}}{\tau_P}.$$
 (3)

Here $D_t \equiv \partial_t + \mathbf{u} \cdot \nabla$, the uniform solvent density $\rho = 1$, α is the coefficient of friction, ν the kinematic viscosity of the fluid, μ the viscosity parameter for the solute (FENE-P), and τ_P the polymer relaxation time;

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	N	L	$ au_P$	$\delta t \times 10^4$	E_{inj}	$\nu \times 10^4$	$\mathcal{W}i$	c	Re_{λ}	$k_{max}\eta_d$
R1	512	6	2	10.0	0.008	10.0	4.71	0.1	107, 85	3.4, 3.6
R2	1024	100	1, 2, 4	1.0	0.005	5.0	$2.26\ 4.52\ 9.04$	0.1	$221,\ 121,\ 53\ ,\ \ 38$	5.1, 5.3, 5.4, 5.5
R3	2048	100	1	1.0	0.003	5.0	1.81	0.4	$147, \ 60$	$14.1, \ 14.8$
R4	2048	100	1	1.0	0.0015	5.0	1.35	0.2	86, 54	$13.2, \ 13.6$
R5	4096	100	1	1.0	0.005	5.0	2.21	0.2	233, 91	20.2, 20.9
R6	4096	100	1	1.0	0.002	5.0	1.53	$0.2 \ 0.4$	$108, \ 62, \ 45$	$24.8, \ 25.8, \ 26.1$
R7	4096	10	1	1.0	0.002	5.0	1.53	0.4	108, 90	24.8, 26.2
R8	4096	100	1	0.5	0.005	1.0	2.91	$0.1 \ 0.4$	$1451,\ 1367,\ 1311$	$8.0, \ 8.3, \ 8.5$
R9	4096	10	1	0.5	0.005	1.0	2.91	0.1	$1451, \ 1407$	8.0, 8.2
R10	16384	100	1	0.5	0.002	5.0	1.56	0.2	$106, \ 61$	$96.4, \ 102.7$

TABLE I: Parameters for our DNS runs R1-R10 with the friction coefficient $\alpha = 0.01$. N^2 is the number of collocation points, δt the time step, E_{inj} the energy-injection rate, ν the kinematic viscosity, and c the concentration parameter. The Taylor-microscale Reynolds number is $Re_{\lambda} \equiv u_{rms}\lambda/\nu$, where $\lambda = (\int E(k)dk/\int k^2 E(k)dk)^{1/2}$ and the Weissenberg number is $Wi \equiv \tau_P \sqrt{\epsilon f/\nu}$, where ϵ^f is the energy dissipation rate per unit mass for the fluid. The dissipation scale is $\eta_d \equiv (\nu^3/\epsilon)^{1/4}$ and $k_{max} = N/3$.

to mimic experiments [16], we use a Kolmogorov-type forcing $F_{\omega} \equiv k_{inj}F_0 \cos(k_{inj}y)$, with amplitude F_0 ; the energy-injection wave vector is k_{inj} (the length scale $l_{inj} \equiv 2\pi/k_{inj}$); the superscript T denotes a transpose, $C_{\beta\gamma} \equiv \langle R_{\beta}R_{\gamma} \rangle$ are the elements of the polymerconformation tensor (angular brackets indicate an average over polymer configurations), \mathcal{I} is the identity tensor, $f(r_P) \equiv (L^2 - 2)/(L^2 - r_P^2)$ is the FENE-P potential, and $r_P \equiv \sqrt{\text{Tr}(\mathcal{C})}$ and L are, respectively, the length and the maximal possible extension of the polymers; and $c \equiv \mu/(\nu + \mu)$ is a dimensionless measure of the polymer concentration [24].

We use periodic boundary conditions, a square simulation domain with side $\mathbb{L} = 2\pi$ and N^2 collocation points, a fourth-order, Runge-Kutta scheme, with time step δt , for time marching, an explicit, fourthorder, central-finite-difference scheme in space, and the Kurganov-Tadmor (KT) shock-capturing scheme [25] for the advection term in Eq. (3); the KT scheme (Eq. (7)) of Ref. [8]) resolves sharp gradients in $\mathcal{C}_{\beta\gamma}$ and thus minimizes dispersion errors, which increase with L and τ_P . We solve Eq. (2) in Fourier space by using the FFTW library [26]. We choose $\delta t \simeq 10^{-3}$ to 5×10^{-5} so that r_P does not become larger than L (Table I). We preserve the symmetric-positive-definite (SPD) nature of \mathcal{C} by adapting to 2D the Cholesky-decomposition scheme of Refs. [7, 8, 24]: We define $\mathcal{J} \equiv f(r_P)\mathcal{C}$, so Eq. (3) becomes

$$D_t \mathcal{J} = \mathcal{J} \cdot (\nabla \mathbf{u}) + (\nabla \mathbf{u})^T \cdot \mathcal{J} - s(\mathcal{J} - \mathcal{I}) + q\mathcal{J}, \quad (4)$$

where $s = (L^2 - 2 + j^2)/(\tau_P L^2)$, $q = [d/(L^2 - 2) - (L^2 - 2 + j^2)(j^2 - 2)/(\tau_P L^2(L^2 - 2))]$, $j^2 \equiv Tr(\mathcal{J})$, and $d = Tr[\mathcal{J}.(\nabla \mathbf{u}) + (\nabla \mathbf{u})^T.\mathcal{J}]$. Given that \mathcal{C} and hence \mathcal{J} are SPD matrices, we can write $\mathcal{J} = \mathcal{LL}^T$, where \mathcal{L} is a lower-triangular matrix with elements ℓ_{ij} , such that $\ell_{ij} =$

0 for j > i; Eq.(4) now yields $(1 \le i \le 2 \text{ and } \Gamma_{ij} \equiv \partial_i u_j)$

$$D_{t}\ell_{11} = \Gamma_{11}\ell_{11} + \Gamma_{21}\ell_{21} + \frac{1}{2}\Big[(q-s)\ell_{11} + \frac{s}{\ell_{11}}\Big],$$

$$D_{t}\ell_{21} = \Gamma_{12}\ell_{11} + \Gamma_{21}\frac{\ell_{22}^{2}}{\ell_{11}} + \Gamma_{22}\ell_{21}$$

$$+ \frac{1}{2}\Big[(q-s)\ell_{21} - s\frac{\ell_{21}}{\ell_{11}^{2}}\Big],$$

$$D_{t}\ell_{22} = -\Gamma_{21}\frac{\ell_{21}\ell_{22}}{\ell_{11}} + \Gamma_{22}\ell_{22}$$

$$+ \frac{1}{2}\Big[(q-s)\ell_{22} - \frac{s}{\ell_{22}}\left(1 + \frac{\ell_{21}^{2}}{\ell_{11}^{2}}\right)\Big].$$
 (5)

Equation(5) preserves the SPD nature of C if $\ell_{ii} > 0$, which we enforce [7, 8] by considering the evolution of $\ln(\ell_{ii})$ instead of ℓ_{ii} .

We have tested explicitly that the statistical properties we measure do not depend on the resolutions we use for our DNS. We check this both by increasing and decreasing this resolution. Indeed, our DNS uses the highest resolution that has been attempted so far for this problem (it uses 256 times as many collocation points as those in Ref. [18]). Furthermore, the Kurganov-Tadmor shock-capturing scheme that we use controls any dispersive errors, because of sharp gradients in the polymer-conformation tensor, as in similar threedimensional studies [7, 24].

We maintain a constant energy-injection rate $E_{inj} \equiv \langle \mathbf{F_u} \cdot \mathbf{u} \rangle$ with $F_{\omega} = \nabla \times \mathbf{F_u}$; the system attains a nonequilibrium, statistically steady state after $\simeq 2\tau_e - 3\tau_e$, where the box-size eddy-turnover time $\tau_e \equiv \mathbb{L}/u_{rms}$ and u_{rms} is the root-mean-square velocity.

In addition to $\boldsymbol{\omega}(\mathbf{x},t)$, $\boldsymbol{\psi}(\mathbf{x},t)$, and $\mathcal{C}(\mathbf{x},t)$ we obtain $\mathbf{u}(\mathbf{x},t)$, the fluid-energy spectrum $E(k) \equiv \sum_{k-1/2 < k' \le k+1/2} k'^2 \langle |\hat{\psi}(\mathbf{k}',t)|^2 \rangle_t$, where $\langle \rangle_t$ indicates a time average over the statistically steady state, the total kinetic energy $\mathcal{E}(t) \equiv \langle \frac{1}{2} | \mathbf{u}(\mathbf{x},t) |^2 \rangle_{\mathbf{x}}$, enstro-



FIG. 1: (Color online) (a) Plots versus time t/τ_e of the total kinetic energy \mathcal{E} of the fluid (top panel), the enstrophy Ω (middle panel), and the palinstrophy \mathcal{P} (bottom panel) for c = 0 (upper curve, blue circles for run R7) and c = 0.4 (lower curve, black line for run R7); (b) log-log (base 10) plots of the energy spectra E(k) versus k for c = 0.2 (red triangles for run R10) and c = 0 (blue circles for run R10); (c) polymer contribution to the scale-dependent viscosity $\Delta\nu(k)$ versus k for c = 0.2 (red line for run R10), $\Delta\nu(k) = 0$ is shown as black dotted line; and (d) energy flux $\Pi(k)$ versus k for c = 0.2 (red dotted line for run R10) and c = 0 (blue line for run R10).

phy $\Omega(t) \equiv \langle \frac{1}{2} | \boldsymbol{\omega}(\mathbf{x}, t) |^2 \rangle_{\mathbf{x}}$, and palinstrophy $\mathcal{P}(t) \equiv \langle \frac{1}{2} | \nabla \times \boldsymbol{\omega}(\mathbf{x}, t) |^2 \rangle_{\mathbf{x}}$, where $\langle \rangle_{\mathbf{x}}$ denotes a spatial average, the PDF of scaled polymer extensions $P(r_P/L)$, the PDFs of ω^2 , σ^2 , and $\Lambda = (\omega^2 - \sigma^2)/8$, where $\sigma^2 \equiv \sum_{ij} \sigma_{ij} \sigma_{ij}$, and $\sigma_{ij} \equiv \partial_i u_j + \partial_j u_i$, the PDF of the Cartesian components of \mathbf{u} , and the joint PDF of Λ and r_P^2 . We obtain the isotropic part of order-p, structure function $S_p(r)$ from longitudinal velocity increments as described in Ref [22]. We concentrate on $S_2(r)$ and the hyperflatness $F_6(r) \equiv S_6(r)/[S_2(r)^3]$; the latter is a measure of the intermittency at the scale r.

III. RESULTS

In Fig. (1a) we show how $\mathcal{E}(t)$ (top panel), $\Omega(t)$ (middle panel), and $\mathcal{P}(t)$ (bottom panel) fluctuate about their mean values $\langle \mathcal{E}(t) \rangle_t$, $\langle \Omega(t) \rangle_t$, and $\langle \mathcal{P}(t) \rangle_t$ for c = 0 (pure fluid) and c = 0.4. Clearly, $\langle \mathcal{E}(t) \rangle_t$, $\langle \Omega(t) \rangle_t$, and $\langle \mathcal{P}(t) \rangle_t$ decrease as c increases. Thus, polymers increase the effective viscosity of the solution; but this naïve conclusion has to be refined, as will be shown later, because the effective viscosity depends on the length scale [6–8].

In Fig. (2a), we plot $S_2(r)$ versus r for c = 0 (blue circles and run R7) and c = 0.2 (green asterisks and run R7); the dashed line, with slope 2, is shown to guide the eye; this slope agrees with the $S_2(r) \sim r^2$ form that we expect, at small r, by Taylor expansion. At large values



FIG. 2: (Color online) (a) Plots of the second-order velocity structure function $S_2(r)$ versus r for c = 0 (blue circle for run **R7**) and c = 0.2 (green asterisks for run **R7**); the line with slope 2 is shown for comparison; (b) plots of the hyperflatness $F_6(r)$ versus r for c = 0 (blue circles for run R7) and c = 0.2 (green asterisks for run R7).

of r, $S_2(r)$ deviates from this r^2 behavior, more so for c = 0.2 than for c = 0, in accord with experiments [16]. Plots of $F_6(r)$ versus r (Fig. (2b)), for c = 0 (blue circles) and c = 0.2 (green asterisks and run R8), show that, on the addition of polymers, small-scale intermittency decreases as c increases.

In Fig. (3a), we show how $E^{p}(k)$ changes, as we increase c: at low and intermediate values of k (e.g., k = 1and 30, respectively), $E^{p}(k)$ decreases as c increases; but, for large values of k (e.g., k = 100), it increases with c. Figure (3b) shows how $E^p(k)$ changes, as we increase τ_P with c held fixed at 0.1. At low values of k (e.g., k = 1), $E^p(k)$ decreases as τ_P increases; but for large values of k (e.g., k = 100) it increases with τ_P .

In Fig. (4a) we give plots, for c = 0.1, of the spectra $E^{p}(k)$ for L = 100 (red triangles and run R8) and L = 10(green asterisks and run R9); for comparison we also plot $E^{f}(k)$ for c = 0; as L increases, the difference between $E^{p}(k)$ and $E^{f}(k)$ increases at large values of k. We see that the larger the value of L the more pronounced is the rise of the large-k tail of $E^{p}(k)$ (cf. the plots in Fig. (4a) with red triangles and green asterisks for L = 100 and L = 10, respectively).

We can understand these trends qualitatively by noting that, even at maximal extension, the size of a polymer is $\leq \eta$ (the dissipation scale). Thus, the polymers stretch at the expense of the fluid energy, which cascades from the intermediate length scales to dissipative scales; this leads to a reduction of E(k) at the values of k that correspond to these intermediate scales. As the polymers relax, they feed energy to the fluid at the deep-dissipation, i.e., large-k, scales; this leads to an enhancement in the tail of E(k) at large values of k. The reduction of energy in the inverse-cascade, low-k regime can be understood by noting that polymers enhance the overall, effective viscosity of the fluid. Indeed, in the limit $\tau_P \to 0$,

 $u \nabla^2 \mathbf{u} + \frac{\mu}{\tau_P} \nabla \cdot f(r_P) C \rightarrow (\nu + \mu) \nabla^2 \mathbf{u} \quad [27].$ To understand quantitatively the effect of polymers on E(k), in different regimes of k, we must compare the fluid-energy spectra, with and without polymers (Fig. (1b)). This leads us naturally to define [6-8] the effective, scale-dependent viscosity $\nu_e(k) \equiv \nu + \Delta \nu(k)$, with

$$\Delta\nu(k) \equiv -\mu \sum_{k-1/2 < k' \le k+1/2} \frac{\mathbf{u}_{\mathbf{k}'} \cdot (\nabla \cdot \mathcal{J})_{-\mathbf{k}'}}{[\tau_P k^2 E^p(k)]} \quad (6)$$

and $(\nabla \cdot \mathcal{J})_{\mathbf{k}}$ the Fourier transform of $\nabla \cdot \mathcal{J}$. Figure (1c) shows that $\Delta \nu(k) > 0$ for k < 30, where $E^p(k) <$ $E^{f}(k)$, whereas, for large values of k, $\Delta\nu(k) < 0$, where $E^{p}(k) > E^{f}(k)$; the superscripts f and p stand, respectively, for the fluid without and with polymers. To understand this dependence on L we plot, in Fig. (4b), the scale-dependent viscosity $\Delta \nu$ for these two representative values, namely, L = 100 (red triangles and run R8) and L = 10 (green asterisks and run R9). We find that $\Delta \nu$ is positive and higher for L = 100, at small values of k, than its counterpart for L = 10; this explains why $E^p(k)$ is smaller for L = 100 than for L = 10 at small k. For large values of k, $\Delta \nu$ is more negative for L = 100than for L = 10, so $E^{p}(k)$ is larger for L = 100 than for L = 10. Note that $\Delta \nu(k)$ changes its sign, from positive to negative, at a smaller value of k for L = 100 than for L = 10; therefore, the large-k tail of $E^{p}(k)$ rises above that of $E^{f}(k)$ at a smaller value of k for L = 100 than for L = 10. By using $\nu_e(k)$, which we obtain from our NS+FENE-P run R7, we carry out a DNS of the NS equation with ν replaced by $\nu_e(k)$; in Fig. 5 we present plots of the energy (left panel), energy spectra (middle panel), PDFs of Λ (right panel and Fig. 8), to compare the results of this DNS with those of run R7 (NS+FENE-P); the good agreement of these results shows that the NS equation with the scale-dependent viscosity $\nu_e(k)$ cap-



FIG. 3: (Color online) (a) Log-log (base 10) plots of the energy spectra E(k) versus k for c = 0 (blue circles for run R6), c = 0.2 (red triangles for run R6), and c = 0.4 (black squares for run R6); plots of E(k) versus c for Wi = 1.53 and k = 1 (left bottom inset), Wi = 1.53 and k = 30 (left top inset), and Wi = 1.53 and k = 100 (right top inset); (b) log-log (base 10) plots of E(k) versus k for Wi = 2.26 (blue circles for run R2), Wi = 4.52 (red triangles for run R2), and Wi = 9.04 (black squares for run R2); plots of E(k) versus τ_P for c = 0.4 and k = 1 (left bottom inset) and c = 0.4 and k = 100 (right top inset).



FIG. 4: (Color online) (a) Log-log (base 10) plots, for c = 0.2 and Wi = 2.91, of E(k) versus k for L = 100 (red triangles for run R8) and L = 10 (green asterisks for run R9); and E(k) for c = 0 (blue circles for run R8); (b) plots, for L = 100 (red triangles for run R8) and L = 10 (green asterisks for run R9), of the scale-dependent correction to the viscosity $\Delta\nu(k)$ versus k.

tures the essential effects of polymer additives on fluid turbulence in run R7 (NS+FENE-P). The form of our effective viscosity indicates that, at large length scales, in addition to the friction, polymers also provide a dissipative mechanism. By contrast, at small length scales, polymers inject energy back into the fluid.

Figure (1d) shows the suppression, by polymer additives, of $\Pi(k) = \int_{k'}^{\infty} T(k') dk'$, where $T(k) = \int \hat{u}_i(-\mathbf{k}) P_{ij}(\mathbf{k}) (\mathbf{u} \times \boldsymbol{\omega})_j(\mathbf{k}) d\Omega$ and $P_{ij}(\mathbf{k}) = \delta_{ij} - \frac{k_i k_j}{k^2}$. The suppression of the spectrum in the small-k régime, which has also been seen in experiments [14] and lowresolution DNS (Fig. (4.12) of Ref. [17]), signifies a reduction of the inverse cascade; the enhancement of the spectrum in the large-k régime leads to the reduction in Ω and \mathcal{P} shown in Fig. (1a); to identify this enhancement unambigouosly requires the run R10, which is by far the highest-resolution DNS of Eqs. (1)-(3) (with 256 times more collocation points than, say, Ref. [18]).

We now plot the PDF $P(r_P/L)$ versus r_P/L in Fig. (6) for c = 0.1 and L = 100 (red triangles and run R8), c = 0.4 and L = 100 (black squares and run R8), and c = 0.1 and L = 10 (green asterisks and run R9). The



FIG. 5: (Color online) Plots with comparisons of the energy (a), energy spectra (b), and the PDF of Λ (c) from our DNS of the NS equations with the *scale-dependent* viscosity $\nu_e(k)$ (black squares) and from the NS+FENE-P run **R7** (green stars). (We calculate $\nu_e(k) \equiv \nu + \Delta\nu(k)$ by substituting our data from run **R7** into Eq. (6).) For reference, we also give plots of all these quantities for the NS equation with conventional, *scale-independent* viscosity (blue circles).



FIG. 6: (Color online) PDFs of the scaled polymer extensions $P(r_P/L)$ versus r_P/L for c = 0.1 and L = 100 (red triangles for run R8), c = 0.4 (black squares for run R8), c = 0.1 and L = 10 (green asterisks for run R9), and c = 0.1 and L = 6 (brown dots for run R1).

extension of the polymers is bounded between $\sqrt{2} \leq r_P \leq L$. The lower bound, $r_P = \sqrt{2}$, corresponds to polymers in a coiled state; near the upper bound, with $r_P \sim L$, the polymers are in a stretched state. In Fig. (6), we show that $P(r_P/L)$ shows a distinct, power-law regime, with exponents that depends on c, L, and Wi. As Wiincreases, this exponent can go from a negative value to a positive value, thus signalling a coil-stretch transition.

In Figs. (7a), (7b), and (7c) we present PDFs of Λ , σ^2 , and ω^2 , respectively, for c = 0 (blue circles and run R7) and c = 0.2 (red triangles and run R7) to show that the addition of polymers suppresses large values of Λ , σ^2 , and ω^2 . If we make scaled plots of PDFs such as $P(\Lambda/\Lambda_{rms})$, then they fall on top of each other for different values of c; this also holds for $P(\sigma^2/\sigma_{rms}^2)$ and $P(\omega^2/\omega_{rms}^2)$. The inset of Fig. (7c) shows that the PDF of any Cartesian component of **u** is very close to a Gaussian. The Fig.(8a) shows a conditional PDF of (r_P/L) conditioned on Λ for run R9; this illustrates that polymers stretch predominantly in strain-dominated regions; this is evident very strikingly in Fig. (8b), which contains a superimposition of contours of r_P^2 on a pseudocolor plot of Λ (for a video sequence of such plots see [28]).

IV. CONCLUSIONS

We have carried out the most extensive and highresolution DNS of 2D, homogeneous, isotropic fluid turbulence with polymer additives. We have used the incompressible, 2D NS equation with air-drag-induced friction and polymer additives; the latter have been modelled by using the finitely-extensible-nonlinear-elastic-Peterlin (FENE-P) model for the polymer-conformation tensor. We find that the inverse-cascade part of the energy spectrum in 2D fluid turbulence is suppressed by the addition of polymers. We demonstrate, for the first time, that the effect of polymers on the forward-cascade part of the fluid energy spectrum in 2D is (a) a slight reduction at intermediate wave numbers and (b) a significant enhancement in the large-wave-number range, as in 3D: these features are resolved unambiguously by our high-resolution DNS. In addition, we find dissipationreduction-type phenomena [7, 8]: polymers reduce the total fluid energy and energy- and mean-square-vorticityor enstrophy-dissipation rates. However, as we have emphasized above, dissipation reduction is not the only notable effect of polymer additives; our extensive, highresolution DNS of 2D fluid turbulence with polymer additives yields good qualitative agreement, in the low-krégime, with the fluid-energy spectra of Ref. [14], and the $S_2(r)$ of Ref. [16]. In addition, our study obtains new results and insights that will, we hope, stimulate new experiments, which should be able to measure (a) the reduction of $\langle \mathcal{E}(t) \rangle_t$, $\langle \Omega(t) \rangle_t$, and $\langle \mathcal{P}(t) \rangle_t$ (Fig.(1a)), (b) the modification of $E^{p}(k)$ at large k (Fig.(1b)), (c) the c, τ_P and L dependences of $E^p(k)$ (Figs.(3a),(3b)



FIG. 7: (Color online) Probability distribution functions (PDFs) of (a) the Okubo-Weiss parameter Λ for run R7, (b) σ^2 for run R7, and (c) ω^2 [inset: a PDF of the velocity component u_x for c = 0 (blue circles for run R7) with a fit (1/2) exp($-u_x^2/12.5$) (blue solid line), and for c = 0.2 (green asterisks for run R7) with a fit (1/2.65) exp($-u_x^2/20$) (green solid line) (note that the addition of polymers reduces the rms value of u_x)].



FIG. 8: (Color online) (a) Conditional PDF of (r_P/L) conditioned on Λ for run R9), (b) a pseudocolor plot of Λ superimposed on a contour plot of r_P^2 for run R10.

and (4a)), (d) the PDFs of (r_P/L) , Λ , σ^2 , and ω^2 , (e) the stretching of polymers in strain-dominated regions (Fig. (8b)), and (f) the suppression of $F_6(r)$ at small r (Fig. (2)).

Two-dimensional fluid turbulence with polymer additives has been studied in channel flows, both in experiments [15] and via DNS [20]; this DNS study uses the Oldroyd-B model, which does not have a maximalpolymer-extension length and is, therefore, less realistic than the FENE-P model we use. These studies obtain energy spectra and second-order structure functions that are qualitatively similar to those we obtain, except at small length scales, which are not resolved in these channel-flow studies. This shows, therefore, that energy spectra and structure functions, obtained far away from walls, are not affected significantly by the walls. Thus, our studies are relevant to the bulk parts of wall-bounded flows too.

V. ACKNOWLEDGMENTS

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- [28] See Supplemental Material at URL for the Video sequence showing pseudocolor plots of the Okubo-Weiss parameter Λ superimposed on contour plots of r_P^2 , which measures the polymer extension. Note that polymers stretch predominantly in the strain-dominated regions of the flow.